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09/890129

PATENT COOPERATION TREATY

From the INTERNATIONAL BUREAU

PCT

NOTIFICATION OF THE RECORDING OF A CHANGE

(PCT Rule 92bis.1 and Administrative Instructions, Section 422)

CIBA SPECIALTY CHEMICALS WATER
TREATMENTS LIMITED
Patents Department
Cleckheaton Road, Low Moor
Bradford
West Yorkshire BD12 0JZ
ROYAUME-UNI

Date of mailing (day/month/year) 26 July 2002 (26.07.02)	ROYA	AUME-UNI	
Applicant's or agent's file reference 21923/AC 533		- IMPORTANT NOTI	FICATION
International application No. PCT/EP01/00391	1	nal filing date (day/month/ye anuary 2001 (15.01.01)	
The following indications appeared on record concerning: X the applicant X the inventor	the agen	t the commo	on representative
Name and Address RAISTRICK Lee		State of Nationality GB Telephone No.	State of Residence GB
Allerton Bradford West Yorkshire BD15 7WJ United Kingdom	===	Facsimile No.	
		Teleprinter No.	
2. The International Bureau hereby notifies the applicant that to the person the name X the add	r	change has been recorded the nationality	concerning: the residence
Name and Address RAISTRICK, Lee		State of Nationality GB	State of Residence GB
78 Sefton Ävenue Hove Edge Brighouse		Telephone No.	
West Yorkshire HD6 2NA United Kingdom		Facsimile No.	3
		Teleprinter No.	SED CK/
3. Further observations, if necessary:			SED CENT
4. A copy of this notification has been sent to:			-0
X the receiving Office the International Searching Authority		the designated Offices X the elected Offices cor	s concernea
the International Preliminary Examining Authority		other:	
	Authorized	l officer	

Facsimile No.: (41-22) 740.14.35

The International Bureau of WIPO 34, chemin des Colombettes

1211 Geneva 20, Switzerland

Lazar Joseph PANAKAL

Telephone No.: (41-22) 338.83.38

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PATENT COOPERATION TREATY

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INTERNATIONAL PRELIMINARY EXAMINATION REPORT

(PCT Article 36 and Rule 70)

Applicant	s or ac	ent's file reference	-	·	
21923/			FOR FURTHER ACT	ON See Notific	cation of Transmittal of International y Examination Report (Form PCT/IPEA/416)
Internation	nal app	olication No.	International filing date (day	/month/vear)	Priority date (day/month/year)
PCT/EP			15/01/2001		28/01/2000
Internation C08F2/4		ent Classification (IPC) or nat	ional classification and IPC		
Applicant					
	PECI	ALTY CHEMICALS WA	TER TREATMENTS Ltd		
1. This and i	intern s tran	ational preliminary exami smitted to the applicant a	nation report has been pre coording to Article 36.	pared by this Inte	ernational Preliminary Examining Authority
2. This	REPO	ORT consists of a total of	4 sheets, including this co	ver sheet.	
l t	peen a	amended and are the basi	by ANNEXES, i.e. sheets s for this report and/or she 7 of the Administrative Ins	ets containing re	n, claims and/or drawings which have ctifications made before this Authority e PCT).
Thes	e ann	exes consist of a total of	sheets.		RECEIVED
<u></u>	··· <u>.</u>				MAR 1 1 2002
3. This	report	contains indications relati	ing to the following items:		TC 1700
ı	\boxtimes	Basis of the report			
Н		Priority			
Ħ		Non-establishment of op	inion with regard to novelt	y, inventive step a	and industrial applicability
IV		Lack of unity of invention			
V	×	Reasoned statement und citations and explanation	der Article 35(2) with regar is suporting such stateme	d to novelty, inve	ntive step or industrial applicability;
VI		Certain documents cited		•••	
VII		Certain defects in the inte	ernational application	-	
VIII	\boxtimes		the international application	n .	
Date of sub	missio	n of the demand	Da	te of completion of t	his report
08/08/20	01				
Name and preliminary	exami	address of the international ning authority:	Au	horized officer	STOCKES MILITARY
<i>၍</i>)	D-80 Tel	pean Patent Office 298 Munich -49 89 2399 - 0 Tx: 523656 e	spmu d	nmerl, R	
	Fax:	+49 89 2399 - 4465	Tal	ephone No. +49 89	0000 0545

INTERNATIONAL PRELIMINARY EXAMINATION REPORT

International application No. PCT/EP01/00391

 Basis of the repe 	.	Bas	is (of :	the	re	poi	rt
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1	the an	e receiving Office in .	nents of the international application (Replacement sheets which have been furnished to response to an invitation under Article 14 are referred to in this report as "originally filed" of this report since they do not contain amendments (Rules 70.16 and 70.17)):
	1-1	13	as originally filed
	Cla	aims, No.:	
	1-1	19	as originally filed
2.	Wit	th regard to the lang guage in which the i	uage, all the elements marked above were available or furnished to this Authority in the nternational application was filed, unless otherwise indicated under this item.
	The	ese elements were a	vailable or furnished to this Authority in the following language: , which is:
		the language of pu	ranslation furnished for the purposes of the international search (under Rule 23.1(b)). blication of the international application (under Rule 48.3(b)). ranslation furnished for the purposes of international preliminary examination (under Rule
3.	Wit	h regard to any nuc l	eotide and/or amino acid sequence disclosed in the international application, the examination was carried out on the basis of the sequence listing:
		contained in the int	ernational application in written form.
		filed together with t	he international application in computer readable form.
		furnished subseque	ently to this Authority in written form.
		furnished subseque	ently to this Authority in computer readable form.
		The statement that the international ap	the subsequently furnished written sequence listing does not go beyond the disclosure in plication as filed has been furnished.
		The statement that listing has been furn	the information recorded in computer readable form is identical to the written sequence nished.
1.	The	amendments have	resulted in the cancellation of:
		the description,	pages:
		the claims,	Nos.:
		the drawings,	sheets:
5.		This report has bee considered to go be	n established as if (some of) the amendments had not been made, since they have been eyond the disclosure as filed (Rule 70.2(c)):

INTERNATIONAL PRELIMINARY EXAMINATION REPORT

International application No. PCT/EP01/00391

(Any replacement sheet containing such amendments must be referred to under item 1 and annexed to this report.)

- 6. Additional observations, if necessary:
- V. Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement
- 1. Statement

Novelty (N)

Yes:

Claims 1-18

No:

Claims 19

Inventive step (IS)

Yes:

Claims 1-18

No:

Claims 19

Industrial applicability (IA)

Yes:

Claims 1-19

No: Claims

2. Citations and explanations see separate sheet

VIII. Certain observations on the international application

The following observations on the clarity of the claims; description, and drawings or on the question whether the claims are fully supported by the description, are made: see separate sheet

Ad section V.:

1. The subject-matter of claims 1-18 is novel and based on an inventive step (Art. 33(2) and (3) PCT).

Document US-A-5 185 385 (D1) describes a polymerization process which is a combination of a photochemical and a thermal process. In the first step, the monomers are polymerized photochemically. This brings the temperature of the monomer mixture to the temperature required for the chemical initiator to dissociate into free radicals.

D1 neither discloses nor suggest the present process wherein a monomer mixture comprising an ultra violet initiator is polymerized thermally in the absence of ultra violet radiation and wherein the formed polymer is post-treated with ultra-violet radiation. This leads to a reduction of residual monomer which problem is not mentioned in D1.

- 2. Independent product claim 19 is not novel (Art. 33(2) PCT). It should be noted that product is not rendered novel merely by the fact that it is produced by means of a new process. At present, there is no indication that the present products are different in any respect from those described in D1 or from any other water soluble or water swellable polymer known in the art.
- 3. Industrial Applicability (Art. 33(4) PCT): o.k.

Ad section VIII.:

1. Independent claim 17 contains all features of independent claim 1 but does not contain a corresponding reference (Rule 6.4 PCT).





PCT

INTERNATIONAL SEARCH REPORT

(PCT Article 18 and Rules 43 and 44)

Applicant's or agent's file reference 21923/AC 533	FOR FURTHER ACTION			ational Search Report applicable, item 5 below.
International application No.	International filing date (da	ny/month/year)	(Earliest) Priority D	ate (day/month/year)
PCT/EP 01/00391	15/01/20	01	28/	01/2000
CIBA SPECIALTY CHEMICALS This International Search Report has bee according to Article 18. A copy is being tra	n prepared by this Internatio	nal Searching Auth	ority and is transmitte	d to the applicant
This International Search Report consists		sheets.	report.	
Basis of the report a. With regard to the language, the language in which it was filed, units and the language in which it was filed, units and the language in which it was filed, units and the language.			is of the international	application in the
the international search w Authority (Rule 23.1(b)).	as carried out on the basis	of a translation of th	e international applic	ation furnished to this
filed together with the inte	e sequence listing: onal application in written for ernational application in com o this Authority in written for o this Authority in computer r osequently furnished written as filed has been furnished.	m. puter readable form n. eadble form. sequence listing do ter readable form is	nes not go beyond the	
3. Unity of invention is lace	•	1).		
4. With regard to the title, X the text is approved as su the text has been established.	ubmitted by the applicant. shed by this Authority to read	d as follows:		
the text has been establis	ubmitted by the applicant. shed, according to Rule 38.2 e date of mailing of this inter	(b), by this Authorit national search rep	y as it appears in Boo ort, submit comments	त् ।।।. The applicant may, s to this Authority.
6. The figure of the drawings to be pub as suggested by the applicant fai because the applicant fai because this figure better	icant.			None of the figures.





Intern: | Application No PCT/EP 01/00391

A. CLASSI IPC 7	FICATION OF SUBJECT MATTER C08F2/48 C08F2/10		
	o International Patent Classification (IPC) or to both national classification	ation and IPC	
	SEARCHED cumentation searched (classification system followed by classification	on symbols)	
IPC 7	C08F C08J`		
Documentat	tion searched other than minimum documentation to the extent that s	such documents are included in the fields sear	ched
Floatura is d	she have executed during the International except from at date he		· .
Electronic d	ata base consulted during the international search (name of data ba	se and, where practical, search terms used)	
		·	
C. DOCUM	ENTS CONSIDERED TO BE RELEVANT		
Category *	Citation of document, with indication, where appropriate, of the rel	evant passages	Relevant to claim No.
A	US 5 185 385 A (R. KANLUEN) 9 February 1993 (1993-02-09)		
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	her documents are listed in the continuation of box C.	Patent family members are listed in	annex.
	ntegories of cited documents:	"T" later document published after the internation or priority date and not in conflict with the	e application but
consid	lered to be of particular relevance document but published on or after the international	cited to understand the principle or theolinvention "X" document of particular relevance; the clai	
	ent which may throw doubts on priority claim(s) or	cannot be considered novel or cannot be involve an inventive step when the docu	e considered to
citatio	is cited to establish the publication date of another n or other special reason (as specified) ent referring to an oral disclosure, use, exhibition or	"Y" document of particular relevance; the clai cannot be considered to involve an inve- document is combined with one or more	ntive step when the
other i	means ent published prior to the international filing date but	ments, such combination being obvious in the art.	to a person skilled
	nan the priority date claimed actual completion of the international search	"&" document member of the same patent fail Date of mailing of the international searce	
	7 April 2001	10/05/2001	•
	mailing address of the ISA	Authorized officer	
	European Patent Office, P.B. 5818 Patentiaan 2 NL ~ 2280 HV Rijswijk		
	Tel. (+31-70) 340-2040, Tx. 31 651 epo nl, Fax: (+31-70) 340-3016	Cauwenberg, C	



INTERNATIONAL SEARCH REP

information on patent family members

Intern: d Application No PCT/EP 01/00391

Patent document cited in search report Publication date Patent family member(s) Publication date

US 5185385 A 09-02-1993 CA 2085619 A 18-06-1994

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- (81) Designated States (national): AE, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CR, CU, CZ, DE, DK, DM, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, UA, UG, US, UZ, VN, YU, ZA, ZW.
- (84) Designated States (regional): ARIPO patent (GH, GM, KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE, TR), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG).

Published:

with international search report

For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

(54) Title: POLYMERISATION PROCESS

(57) Abstract: A process of preparing water soluble or water swellable polymer comprising the steps, (a) forming an aqueous mixture comprising, (i) a water soluble ethylenically unsaturated monomer or blend of monomers and, (ii) an ultra violet initiator, (b) effecting polymerisation by subjecting the aqueous mixture formed in step (a) to polymerisation conditions to form a polymer of said monomer or monomer blend, (c) subjecting the polymer formed in step (b) to ultra violet light radiation, characterised in that the polymerisation step (b) is conducted substantially in the absence of ultra violet radiation. In one preferred aspect the ultra violet initiator is distributed throughout the polymer formed in step (b). In another preferred aspect the step (c) is conducted ultra violet light at an intensity of up to 500 milli Watts/cm². Also claimed is a method of reducing the residual monomer content in a water soluble or water swellable polymer by subjecting the polymer to ultra violet irradiation in the presence of an ultra violet initiator. The process is particularly suitable for making highly effective water soluble and water swellable polymers useful as flocculants, coagulants, rheology modifiers, dispersants, superabsorbents and binders etc.



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Polymerisation Process

The present invention relates to a process for making water soluble or water swellable polymers, by polymerisation of water soluble ethylenically unsaturated monomer or monomer blend. In particular the invention relates to processes of making said polymers containing low concentrations of residual monomer.

Water soluble and water swellable polymers are used in numerous industrial applications, for instance, flocculants, coagulants, rheology modifiers, dispersants, superabsorbents and binders. Of particular importance are high molecular weight water soluble polymeric flocculants which may be used as retention or drainage aids in paper making or to flocculate sludges such as sewage sludge, waste waters, textile industry effluents red mud from the Bayer Alumina process and suspensions of coal tailings etc.

It is standard practice to prepare water soluble or water swellable polymers by polymerising water soluble monomers using a suitable initiator system. The polymers are usually provided either as a solid particulate product or as a reverse phase dispersion or emulsion. Typically particulate polymers are prepared introducing initiators into an aqueous solution of the monomers and polymerising to form a polymer gel which is then cut into smaller pieces, dried and then ground to the appropriate particle size. Alternatively the polymers are produced as beads by suspension polymerisation or as a water-in-oil emulsion or dispersion by water-in-oil emulsion polymerisation, for example according to a process defined by EP-A-150933, EP-A-102760 or EP-A-126528.

It is known to produce water soluble and water swellable polymers using a variety of initiator systems. For instance it is common practice to polymerise water soluble monomers using redox initiator couples, in which radicals are generated by admixing with the monomer a redox couple which is a reducing agent and an oxidising agent. It is also conventional practice to use either alone or in combination with other initiator systems a thermal initiator, which would include



any suitable initiator compound that releases radicals at an elevated temperature. Other initiator systems include photo and radiation induced initiator systems, which require exposure to radiation to release radicals thereby effecting polymerisation. Other initiator systems are well known and well documented in the literature.

Although water soluble and water swellable polymers can be prepared using many of the commercially available initiator systems, it is often difficult to prepare on an industrial scale polymers which have the correct molecular weight in combination with other desired characteristics, such as solubility, degree of absorbency etc. Over the last ten to fifteen years it has also become increasingly important to provide polymers which have extremely low levels of residual free monomer. This is particularly the case for polymers based on acrylamide monomer.

There have been various proposals in the literature for reducing residual free monomer concentrations in polymers, especially polymers of acrylamide. For instance in US-A-4906732 and US-A-4996251 polyacrylamides are treated with an amidase enzyme which is active towards acrylamide. However, although it was possible to achieve very low levels of free acrylamide, the enzymes proposed in these patents cannot consistently especially at elevated temperatures.

WO-A-97 29136 describes an amidase enzyme which is particularly effective at high temperatures and thus can be applied to the hot polymer gel substantially immediately prior to the drying stage. However, although this enzyme has shown particular advantages over other known amidases, it is still nonetheless difficult to consistently achieve low residual levels of acrylamide on an industrial scale.

Therefore there exists a need to be able to conveniently and consistently provide water soluble or swellable polymers with no or extremely low levels of residual monomer, especially acrylamide monomer.



There also exists a need to achieve this in an industrial scale process and in particular in a process which does not require additional long residence stages in the production process.

According to one aspect of the invention we provide a process of preparing water soluble or water swellable polymer comprising the steps,

- (a) forming an aqueous mixture comprising,
 - (i) a water soluble ethylenically unsaturated monomer or blend of monomers and,
 - (ii) an ultra violet initiator,
- (b) effecting polymerisation by subjecting the aqueous mixture formed in step (a) to polymerisation conditions to form a polymer of said monomer or monomer blend, wherein ultra violet initiator is distributed throughout the polymer,
- (c) subjecting the polymer formed in step (b) to ultra violet light radiation, characterised in that the polymerisation step (b) is conducted substantially in the absence of ultra violet radiation.

Although higher levels of ultra violet radiation may be employed generally step (c) is conducted using fairly low levels of ultra violet radiation intensity, for instance up to 1 Watt/cm², usually below 500 milli Watts/cm².

According to a further aspect of the invention we provide a process of preparing water soluble or water swellable polymer comprising the steps,

- (a) forming an aqueous mixture comprising,
 - (i) a water soluble ethylenically unsaturated monomer or blend of monomers and,
 - (ii) an ultra violet initiator,
- (b) effecting polymerisation by subjecting the aqueous mixture formed in step (a) to polymerisation conditions to form a polymer of said monomer or monomer blend,

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(c) subjecting the polymer formed in step (b) to ultra violet light radiation at an intensity of up to 500 milli Watts, characterised in that the polymerisation step (b) is conducted substantially in the absence of ultra violet radiation.

The advantage of being able to use relatively low levels of radiation intensity is that there is a reduced risk of inducing denaturing of the polymer. One effect of denaturing the polymer may be undesirable or uncontrolled cross-linking or unacceptable loss of solubility. This may be particularly important when preparing high molecular weight water soluble polymers, where cross-linking and/or loss of solubility could have a deleterious effect on performance. To a certain extent exposure to high levels of ultra violet radiation may be detrimental to deliberately cross-linked polymers in that the additional cross-linking would be uncontrolled and could also lead to a loss of performance. Thus for a cross-linked superabsorbent polymer excessive exposure to ultra-violet cross-linking may result in excessive cross-linking which could impair the absorbency charactersitics.

Thus it is preferred that very low levels of UV radiation intensity are used, for instance up to 100 milli Watts/cm². Generally the levels of intensity will be above 5 or 10 milli Watts/cm². Intensities of below 50 milli Watts/cm² are generally preferred, for instance in the range of 30 to 40 milliWatts/cm².

The water soluble or water swellable polymer is prepared by polymerisation of a water soluble monomer or water soluble monomer blend. By water soluble we mean that the water soluble monomer or water soluble monomer blend has a solubility in water of at least 5g in 100 ml of water, measured at 25°C. The polymerisation step (b) may employ conventional polymerisation techniques, provided that these do not result in exposure to ultra violet light.

The polymerisation step (b) may be effected by subjecting the aqueous monomer solution to any conventional polymerisation conditions which do not involve exposure to ultra violet radiation. Desirably this may be achieved by the use of



redox initiators and/or thermal initiators. Typically redox initiators include a reducing agent such as sodium sulphite, sulphur dioxide and an oxidising compound such as ammonium persulphate or a suitable peroxy compound, such as tertiary butyl hydroperoxide etc. Redox initiation may employ up to 10,000 ppm (based on weight of monomer) of each component of the redox couple. Preferably though each component of the redox couple is often less than 1000 ppm, typically in the range 1 to 100 ppm, normally in the range 4 to 50 ppm. The ratio of reducing agent to oxidizing agent may be from 10:1 to 1:10, preferably in the range 5:1 to 1:5, more preferably 2:1 to 1:2, for instance around 1:1.

Polymerisation step (b) may also be effected by employing a thermal initiatior alone or in combination with other initiator systems, for instance redox initiators. Thermal initiators would include any suitable initiator compound that releases radicals at an elevated temperature, for instance azo compounds, such as azobisisobutyronitrile (AZDN), 4,4'-azobis-(4-cyanovalereic acid) (ACVA). Typically thermal initiators are used in an amount of up 10,000 ppm, based on weight of monomer. In most cases, however, thermal initiators are used in the range 100 to 5,000 ppm preferably 200 to 2,000 ppm, usually around 1,000 ppm.

The water soluble or water swellable polymer prepared according to the process of the present invention may be cationic, anionic, nonionic or amphoteric. It may be substantially linear or alternatively branched or cross-linked. Cross-linked or branched polymers are prepared by incorporating a branching or cross-linking agent into the monomer blend. The cross-linking or branching agent may be for instance a di- or multifunctional material that reacts with functional groups pendant on the polymer chain, for instance multivalent metal ions or amine compounds which can react with pendant carboxylic groups. Preferably, however, the cross-linking or branching agent will be a polyethylenically unsaturated compound, which becomes polymerised into two or more polymer chains. Typically such cross-linking agents include methylene-bis-acrylamide, tetra allyl ammonium chloride, triallyl amine and polyethylene glycol di acrylate. The polymers may be highly crosslinked and therefore water insoluble but water swellable. Alternatively the

6.

polymer may be water soluble and either substantially linear or slightly branched, for instance prepared using less than 10 ppm cross-linking/branching monomer.

The water soluble or water swellable polymer may be cationic, anionic, amphoteric or non-ionic. Anionic polymers may be formed from one or more ethylenically unsaturated anionic monomers or a blend of one or more anionic monomers with for instance a nonionic monomer, preferably acrylamide. The anionic monomers include acrylic acid, methacrylic acid, maleic acid, crotonic acid, itaconic acid, vinylsulphonic acid, allyl sulphonic acid, 2-acrylamido-2-methylpropane sulphonic acid and salts thereof. A preferred anionic polymer is the copolymer of sodium acrylate with acrylamide.

Cationic polymers may be formed from one or more ethylenically unsaturated cationic monomers optionally with for instance a nonionic monomer, preferably acrylamide. The cationic monomers include dialkylamino alkyl (meth) acrylates, dialkylamino alkyl (meth) acrylamides, including acid addition and quaternary ammonium salts thereof, diallyl dimethyl ammonium chloride. Preferred cationic monomers include the methyl chloride quaternary ammonium salts of dimethylamino ethyl acrylate and dimethyl aminoethyl methacrylate.

Amphoteric polymers include at least one cationic monomer (for example as defined above) and at least one anionic monomer (for example as defined above) optionally with a nonionic monomer, especially acrylamide.

Non-ionic polymers include polymers of any suitable non-ionic monomers, for instance, acrylamide, methacrylamide, N-vinylpyrrolidone and 2-hydroxyethyl acrylate. Preferred non-ionic polymers comprise acrylamide especially acrylamide homopolymers.

Preferably, the water soluble or water swellable polymers comprise acrylamide.



The polymer produced by the process of the present invention may be a relatively low molecular weight polymer, for instance polymerised to a molecular weight below 100,000, for instance 2,000 to 10,000. Preferably however, the polymers are relatively higher molecular weight, for instance at least 100,000, especially at least 500,000. Typically the polymer has a molecular weigh in the range of above 1 million to 20 or 30 million or higher. In general these high molecular weight polymers tend to exhibit high intrinsic viscosities (IV), for instance at least 3 dl/g (measured at various polymer concentrations using standard techniques in 1N NaCl buffered to pH 7.5 at 25°C). Preferably the polymer has an IV of at least 4 dl/g often at least 7 or 8 dl/g, for instance at least 12 dl/g. In some cases it may be highly desirable for the polymer to have an IV as high as 20 or 30 dl/g or even higher. However especially preferred polymers have an IV in the range 8 to 18 dl/g.

Typically an aqueous solution of water soluble monomer may be polymerised by solution polymerisation to provide an aqueous gel or by reverse phase polymerisation in which an aqueous solution of monomer is suspended in a water immiscible liquid and polymerised to form polymeric beads or alternatively by emulsifying aqueous monomer into an organic liquid and then effecting emulsion polymerisation. Examples of reverse phase polymerisation are given in EP-A-150933, EP-A-102760 or EP-A-126528. Preferably the polymer is prepared by solution polymerisation.

The process of the present invention requires that an aqueous monomer mixture is first formed comprising (i) a water soluble ethylenically unsaturated monomer or blend of monomers and (ii) an ultra violet initiator. In addition the aqueous monomer mixture may also contain other components, for instance redox initiators or thermal initiators or other compounds that may assist with the polymerisation step (b). The aqueous monomer mixture may also comprise other ingredients, for instance chain transfer agents which may be required to regulate the chain length.

WO 01/55228

The ultra violet initiator (ii) comprised in the aqueous monomer mixture may be any suitable initiator that remains substantially inert during the polymerisation step (b). Therefore the ultra violet initiator would generally be unsuitable if it decomposed during this initial polymerisation step. Therefore it is desirable to choose an ultra violet initiator that is not temperature sensitive at a temperature reached during the initial polymerisation step.

Desirably the ultra violet initiator is distributed homogenously throughout the aqueous monomer mixture, in order that it is evenly distributed throughout the resulting polymer. Preferably the ultra violet initiator is soluble or dispersible in the aqueous monomer or monomer blend.

We have surprisingly found that effective polymers can be produced by the process of the present invention, wherein an aqueous monomer blend which also contains an ultra violet initiator is first subjected to polymerisation in the absence of ultra violet light in which the ultra violet initiator remains substantially inert and then subjecting the polymer to ultra violet radiation.

Preferably the ultra violet initiator is a compound of formula:

$$R_2$$
 R_1 R_3 R_3

wherein R_1 and R_2 are each independently C_{1-3} alkyl or together form a C_{4-8} cycloaliphatic ring, R_3 is H, C_{1-2} alkyl or $-O(CH_2CH_2)_nOH$ and n is 1-20. An especially preferred ultra violet initiator is the compound defined by the formula,



known as 1-[4-(2-Hydroxyethoxy)-phenyl]-2-hydroxy-2-methyl-1-propane-1-one supplied as Irgacure ® 2959 photoinitiator by Ciba Specialty Chemicals.

Another especially preferred UV initiator is the compound of the formula,

known as 1-phenyl-2-hydroxy-2-methyl-1-propane-1-one supplied as Darocure ® 1173 photoinitiator by Ciba Specialty Chemicals.

Desirably the ultra violet initiator is used in an amount up to 10,000 ppm by weight of monomer. However, for economic reasons it is usually preferred not to use more than about 5,000. Suitable results are often obtained when the ultra violet initiator is included in an amount in the range 50 to 3,000 ppm, more preferably 100 to 2,500 ppm, especially 500 to 2,000 ppm.

The process involves the step of subjecting the polymer formed in the polymerisation step (b) to ultra violet radiation. This may be done by passing the formed polymer under ultra violet lamps. For instance the polymer may be passed from the reactor vessel and then irradiated with a suitable dose of ultra violet light and then passed to a drying section. Alternatively the polymer may be exposed to ultra violet radiation in the reactor vessel. Preferably the polymer is subjected to the ultraviolet light in the drying section. Thus in this preferred form of the invention ultra violet lamps are mounted such that the polymer is exposed to ultra violet light whilst inside the drying equipment. More preferably the drying equipment is a fluid bed dryer and the ultra violet lamps are mounted inside the dryer.

It has further surprisingly been found that a water soluble or water swellable polymer in which the amount of residual monomer is below 100 ppm is obtainable



by the process of the present invention, including any of the more specific embodiments.

According to a further aspect of the invention we provide a method of reducing the residual monomer content in a water soluble or water swellable polymer by subjecting the polymer to ultra violet irradiation in the presence of an ultra violet initiator. The ultra violet initiator may be applied to the surface of the formed polymer and allowed to coat the surface of the polymer particles and then subjecting the polymer to ultra violet radiation. In a preferred form of this aspect of the invention the ultra violet initiator is actually absorbed into the polymer and is then preferably distributed throughout the polymer before being subjected to irradiation by ultra violet light. Alternatively the water soluble or water swellable polymer may be formed containing the ultra violet initiator distributed throughout the polymer. This may be for instance as a result of carrying out a process in accordance with the first aspect of the invention.

Preferably the method of reducing residual monomer is applied to polymers of acrylamide and said acrylamide polymer contains residual acrylamide monomer. More preferably the polymer of acrylamide is a relatively high molecular weight polymer and has an intrinsic viscosity of at least 4 dl/g, often at least 7 or 8 dl/g, for instance at least 12 dl/g. In some cases it may be highly desirable for the polymer of acrylamide to have an IV as high as 20 or 30 dl/g or even higher. Especially preferred are polymers of acrylamides which have an IV in the range 8 to 18 dl/g.

The ultra violet initiator may be any suitable ultra violet initiator as given herein before. It is preferred that the ultra violet initiator is water soluble or at least water dispersible. Preferably the ultra violet initiator is a compound of formula,



$$R_2$$
 R_3
 R_3
 R_3

wherein R_1 and R_2 are each independently C_{1-3} alkyl or together form a C_{4-8} cycloaliphatic ring, R_3 is H, C_{1-2} alkyl or $-O(CH_2CH_2)_nOH$ and n is 1-20. Most preferably the ultra violet initiator either a compound of formula,

or a compound of formula

The following examples illustrate the invention, but are not intended to in any way limit the scope of the invention.



Examples

Test 1

Two tonnes of aqueous monomer mixture is prepared comprising 90% by weight acrylamide and 10% by weight dimethylaminoethyl acrylate methyl chloride quaternary ammonium salt and having a total monomer concentration of about 30%. Nitrogen gas is passed through the aqueous medium in order to remove dissolved oxygen or other volatile reactive species. 4.5 ppm potassium bromate KBrO₃ and 9ppm sodium sulphite Na₂SO₃ is combined with the aqueous monomer and mixed thoroughly. Polymerisation is allowed to proceed for two hours and the resulting polymer is dried using a fluid bed dryer.

Test 2

This is repeated but subjecting the gel to ultra violet radiation for 20 minutes during the drying process using a UV flood system from Starna using an intensity of 2X10⁻⁴µW/cm²/nm. The equivalent irradiation will by obtained using a Solartell Solarscope, model 1 with a multidirectional probe, using an intensity of 25milli Watts/cm². These tests are repeated using various amounts of 1-[4-(2-Hydroxyethoxy)-phenyl]-2-hydroxy-2-methyl-1-propane-1-one (Irgacure ® 2959) in the monomer mixture.

Tests 3 to 6

The solublity, solution viscosity and residual acrylamide monomer are assessed and the results are shown in Table 1.



Table 1

Test	UV initiator	UV irradiation	1% solution	Solubility	Residual
ļ	(ppm)	(min)	viscosity (cP)*		Acrylamide (ppm)
1	0	0	188	Good	881
2	0	20	199	Good	452
3	500	0	194	Good	964
4	500	20	182	Fair/Good	57
5	2000	0	176	Fair/good	960
6	2000	20	166	Good	47

measured using a Mettler viscometer at a shear rate of 30^{-s}, measured at 25°C.

Examples 7 to 12

Examples 1 to 6 are repeated but using a an aqueous solution of acrylamide monomer. Viscosity and residual acrylamide concentrations are shown in Table 2.

Table 2

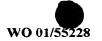
Test	UV initiator	UV irradiation	1% solution	Residual
	(ppm)	(min)	viscosity (cP)#	Acrylamide (ppm)
1	0	0	28	532
2	0	20	24	412
3	500	0	26	552
.4	500	20	24	38
5	2000	0	28	639
6	2000	20	24	32

measured using a Mettler viscometer at a shear rate of 250^{-s}, measured at 25°C.



Claims

- 1. A process of preparing water soluble or water swellable polymer comprising the steps,
 - (a) forming an aqueous mixture comprising,
 - (i) a water soluble ethylenically unsaturated monomer or blend of monomers and,
 - (ii) an ultra violet initiator,
 - (b) effecting polymerisation by subjecting the aqueous mixture formed in step (a) to polymerisation conditions to form a polymer of said monomer or monomer blend, wherein ultra violet initiator is distributed throughout the polymer,
- (c) subjecting the polymer formed in step (b) to ultra violet light radiation, characterised in that the polymerisation step (b) is conducted substantially in the absence of ultra violet radiation.
- 2. A process according to claim 1 in which the polymerisation step (b) is effected by suitable polymerisation initiators, selected from the group consisting of redox initiators and thermal initiators.
- 3. A process according to claim 1 or claim 2 in which the polymer in step (c) is subjected to ultraviolet light radiation at an intensity of up to 500 milliWatts.
- 4. A process according to any of claims 1 to 3 in which the polymer is formed from acrylamide.
- 5. A process according to any of claims 1 to 4 in which the polymer has an intrinsic viscosity of at least 4 dl/g.
- 6. A process according to any of claims 1 to 5 in which the polymer formed by solution polymerisation.
- 7. A process according to any of claims 1 to 6 in which the ultra violet initiator is soluble or dispersible in the aqueous monomer or monomer blend.
- 8. A process according to any of claims 1 to 7 in which the ultra violet initiator is a compound of formula:



$$R_2$$
 R_3
 R_3

wherein R_1 and R_2 are each independently C_{1-3} alkyl or together form a C_{4-8} cycloaliphatic ring, R_3 is H, C_{1-2} alkyl or $-O(CH_2CH_2)_nOH$ and n is 1-20.

9. A process according to claim 8 in which the ultra violet initiator is a compound of formula:

10. A process according to claim 8 in which the ultra violet initiator is a compound of formula:

- 11. A process according to any of claims 1 to 10 in which step (c) is conducted simultaneous with a drying stage.
- 12. A method of reducing the residual monomer content in a water soluble or water swellable polymer by subjecting the polymer to ultra violet irradiation in the presence of an ultra violet initiator.
- 13. A method according to claim 12 in which the polymer is a polymer of acrylamide of intrinsic viscosity above 4 dl/g.
- 14. A method according to claim 12 or claim 13 in which the ultra violet initiator is a compound of formula:

$$R_2$$
 R_1
 R_2
 R_3
 R_3

wherein R_1 and R_2 are each independently $C_{1\text{--}3}$ alkyl or together form a $C_{4\text{--}8}$



cycloaliphatic ring, R₃ is H, C₁₋₂ alkyl or -O(CH₂CH₂)_nOH and n is 1-20.

15. A method according to claim 14 in which the ultra violet initiator is a compound of formula:

16. A method according to claim 15 in which the ultra violet initiator is a compound of formula:

- 17. A process of preparing water soluble or water swellable polymer comprising the steps,
 - (a) forming an aqueous mixture comprising,
 - (i) a water soluble ethylenically unsaturated monomer or blend of monomers and,
 - (ii) an ultra violet initiator,

absence of ultra violet radiation.

- (b) effecting polymerisation by subjecting the aqueous mixture formed in step (a) to polymerisation conditions to form a polymer of said monomer or monomer blend,
- (c) subjecting the polymer formed in step (b) to ultra violet light radiation at an intensity of up to 500 milli Watts, characterised in that the polymerisation step (b) is conducted substantially in the
- 18. A process according to claim 17 in which the ultra violet light radiation is at an intensity of up to 50 milli Watts.
- 19. A water soluble or water swellable polymer obtainable by a process defined by any of claims 1 to 11, 17 or 18 or by a method according to anyone of claims 12 to 16 in which the amount of residual monomer is below 100 ppm.

INTERNATIONAL SEARCH REPORT

Interr nal Application No

	•	PCT	/US 00/25528
A. CLASSI IPC 7	FICATION OF SUBJECT MATTER C08F6/00		
	o International Patent Classification (IPC) or to both national classification	assification and IPC	
	SEARCHED ocumentation searched (classification system followed by class	sification symbols)	
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Documenta	tion searched other than minimum documentation to the extent	that such documents are included in	n the fields searched
Electronic d	lata base consulted during the international search (name of d	ata base and, where practical, search	h terms used)
WPI Da	ta, EPO-Internal		
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C. DOCUM	ENTS CONSIDERED TO BE RELEVANT		
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	abstract; claims; examples 8, page 5, line 48 - line 54	lO; table 1	
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	Section Ch, Week 198236 Derwent Publications Ltd., Lor Class A14, AN 1982-75091E XP002156085		
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X Furt	her documents are listed in the continuation of box C.	Patent family member	ers are listed in annex.
° Special ca	ategories of cited documents:		after the international filing date
A docume	ent defining the general state of the art which is not dered to be of particular relevance		conflict with the application but rinciple or theory underlying the
	document but published on or after the international	"X" document of particular rele	evance; the claimed invention velor cannot be considered to
"L" docume	ent which may throw doubts on priority claim(s) or is cited to establish the publication date of another	involve an inventive step	when the document is taken alone
citatio	n or other special reason (as specified) ent referring to an oral disclosure, use, exhibition or	cannot be considered to	evance; the claimed invention involve an inventive step when the ith one or more other such docu-
other	means ent published prior to the international filing date but		being obvious to a person skilled
latert	han the priority date claimed	*&* document member of the	
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Name and	mailing address of the ISA European Patent Office, P.B. 5818 Patentlaan 2	Authorized officer	
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Interr nal Application No PCT/US 00/25528

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